

# Document made available under the Patent Cooperation Treaty (PCT)

International application number: PCT/US05/005852

International filing date: 24 February 2005 (24.02.2005)

Document type: Certified copy of priority document

Document details: Country/Office: US  
Number: 60/547,853  
Filing date: 26 February 2004 (26.02.2004)

Date of receipt at the International Bureau: 17 March 2005 (17.03.2005)

Remark: Priority document submitted or transmitted to the International Bureau in compliance with Rule 17.1(a) or (b)



World Intellectual Property Organization (WIPO) - Geneva, Switzerland  
Organisation Mondiale de la Propriété Intellectuelle (OMPI) - Genève, Suisse



# THE UNITED STATES OF AMERICA

TO ALL TO WHOM THESE PRESENTS SHALL COME:

UNITED STATES DEPARTMENT OF COMMERCE

United States Patent and Trademark Office

March 09, 2005

THIS IS TO CERTIFY THAT ANNEXED HERETO IS A TRUE COPY FROM THE RECORDS OF THE UNITED STATES PATENT AND TRADEMARK OFFICE OF THOSE PAPERS OF THE BELOW IDENTIFIED PATENT APPLICATION THAT MET THE REQUIREMENTS TO BE GRANTED A FILING DATE.

APPLICATION NUMBER: 60/547,853

FILING DATE: February 26, 2004

RELATED PCT APPLICATION NUMBER: PCT/US05/05852



Certified by

Under Secretary of Commerce  
for Intellectual Property  
and Director of the United States  
Patent and Trademark Office

16509 U.S. PTO  
022604

# PROVISIONAL APPLICATION FOR PATENT COVER SHEET

This is a request for filing a PROVISIONAL APPLICATION FOR PATENT under 37 CFR 1.53(c).

Express Mail Label No. EL 900960546 US

INVENTOR(S)					
Given Name (first and middle (if any))		Family Name or Surname		Residence (City and either State or Foreign Country)	
Richard A. David S.		Brown Robinson		Lawrenceville, NJ Mount Laurel, NJ	
Additional inventors are being named on the _____ separately numbered sheets attached hereto					
TITLE OF THE INVENTION (500 characters max)					
Oxidation of Organic Compounds at High PH					
Direct all correspondence to: CORRESPONDENCE ADDRESS					
<input type="checkbox"/> Customer Number: _____ OR <input checked="" type="checkbox"/> Firm or Individual Name: Patent Administrator, FMC Corporation					
Address: 1735 Market Street					
Address: _____					
City: Philadelphia		State	PA	ZIP	19103
Country: United States of America		Telephone	215-299-6985	Fax	215-299-6984
ENCLOSED APPLICATION PARTS (check all that apply)					
<input checked="" type="checkbox"/> Specification Number of Pages 15			<input type="checkbox"/> CD(s), Number _____		
<input checked="" type="checkbox"/> Drawing(s) Number of Sheets 3			<input checked="" type="checkbox"/> Other (specify) ExpMail Stmt;Postcard		
<input type="checkbox"/> Application Data Sheet. See 37 CFR 1.76					
METHOD OF PAYMENT OF FILING FEES FOR THIS PROVISIONAL APPLICATION FOR PATENT					
<input type="checkbox"/> Applicant claims small entity status. See 37 CFR 1.27. <input type="checkbox"/> A check or money order is enclosed to cover the filing fees. <input checked="" type="checkbox"/> The Director is hereby authorized to charge filing fees or credit any overpayment to Deposit Account Number: 06-1440 <input type="checkbox"/> Payment by credit card. Form PTO-2038 is attached.				FILING FEE Amount (\$)  160.00	
The invention was made by an agency of the United States Government or under a contract with an agency of the United States Government.					
<input checked="" type="checkbox"/> No. <input type="checkbox"/> Yes, the name of the U.S. Government agency and the Government contract number are: _____					

15535 U.S. PTO  
60/547853  
022604

[Page 1 of 1]

Respectfully submitted,

SIGNATURE

*John M. Sheehan*

TYPED or PRINTED NAME John M. Sheehan

TELEPHONE 215-299-6966

Date 02/26/04

REGISTRATION No. 26,065

(If appropriate)

Docket Number: 60376-USA-PROV1

## USE ONLY FOR FILING A PROVISIONAL APPLICATION FOR PATENT

This collection of information is required by 37 CFR 1.51. The information is required to obtain or retain a benefit by the public which is to file (and by the USPTO to process) an application. Confidentiality is governed by 35 U.S.C. 122 and 37 CFR 1.14. This collection is estimated to take 8 hours to complete, including gathering, preparing, and submitting the completed application form to the USPTO. Time will vary depending upon the individual case. Any comments on the amount of time you require to complete this form and/or suggestions for reducing this burden should be sent to the Chief Information Officer, U.S. Patent and Trademark Office, U.S. Department of Commerce, P.O. Box 1450, Alexandria, VA 22313-1450. DO NOT SEND FEES OR COMPLETED FORMS TO THIS ADDRESS. SEND TO: Mail Stop Provisional Application, Commissioner for Patents, P.O. Box 1450, Alexandria, VA 22313-1450.

If you need assistance in completing the form, call 1-800-PTO-9199 and select option 2.

**IN THE UNITED STATES PATENT AND TRADEMARK OFFICE**

In re application of: Richard A. Brown, David S. Robinson

Application No.: to be assigned

Filed: 02/26/2004

For: Oxidation of Organic Compounds at High PH

**Commissioner for Patents  
Alexandria, VA 22313-1450**

**EXPRESS MAIL CERTIFICATE**

"Express Mail" label number EL 900960546 US

Date of Deposit 02/26/2004

I hereby state that the following attached paper or fee

Provisional Patent Application Cover Sheet (1 pg.)

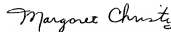
Specification ( 15 pgs.)

Drawings (3 pgs.)

Postcard

Is being deposited with the United States Postal Service "Express Mail Post Office to Addressee" service under 37 C.F.R. section 1.10, on the date indicated above and is addressed to: Mail Stop Provisional Patent Application, Commissioner for Patents, P. O. Box 1450, Alexandria, VA 22313-1450.

Margaret Christy



Signature of person mailing paper or fee

## OXIDATION OF ORGANIC COMPOUNDS AT HIGH PH

## FIELD OF THE INVENTION

5

The present invention relates to the in situ and ex situ oxidation of organic compounds in soils, groundwater, process water and wastewater and especially relates to the in situ oxidation of volatile and semi-volatile organic compounds, pesticides and herbicides, and other recalcitrant organic compounds in soil and groundwater.

10

## BACKGROUND OF THE INVENTION

The presence of volatile organic compounds (VOCs), semi volatile organic compounds (SVOCs) or pesticides in subsurface soils and groundwater is a well-  
15 documented and extensive problem in industrialized and industrializing countries. Many VOC's and SVOC's are compounds which are toxic or carcinogenic, are often capable of moving through the soil under the influence of gravity and serving as a source of water contamination by dissolution into water passing through the contaminated soil. These include, but are not limited to, chlorinated solvents such  
20 as trichloroethylene (TCE), vinyl chloride, tetrachloroethylene (PCE), methylene chloride, 1,2-dichloroethane (DCA), 1,1,1-trichloroethane (TCA), carbon tetrachloride, chloroform, chlorobenzenes, benzene, toluene, xylene, ethyl benzene, ethylene dibromide, methyl tertiary butyl ether, polyaromatic hydrocarbons, polychlorobiphenyls, phthalates, 1,4-dioxane, nitrosodimethyl  
25 amine, and methyl tertbutyl ether.

In many cases discharge of these compounds into the soil leads to contamination of aquifers resulting in potential public health impacts and degradation of groundwater resources for future use. Treatment and remediation of soils  
30 contaminated with VOC or SVOC compounds have been expensive, require considerable time, and in many cases incomplete or unsuccessful. Treatment and

remediation of volatile organic compounds that are either partially or completely immiscible with water (i.e., Non Aqueous Phase Liquids or NAPLs) have been particularly difficult. Also treatment of highly soluble but biologically stable organic contaminants such as MTBE and 1,4-dioxane are also quite difficult with conventional remediation technologies. This is particularly true if these compounds are not significantly naturally degraded, either chemically or biologically, in soil environments. NAPLs present in the subsurface can be toxic to humans and other organisms and can slowly release dissolved aqueous or gas phase volatile organic compounds to the groundwater resulting in long-term (i.e., decades or longer) sources of chemical contamination of the subsurface. In many cases subsurface groundwater contaminant plumes may extend hundreds to thousands of feet from the source of the chemicals resulting in extensive contamination of the subsurface. These chemicals may then be transported into drinking water sources, lakes, rivers, and even basements of homes through volatilization from groundwater.

15

The U.S. Environmental Protection Agency (USEPA) has established maximum concentration limits for various hazardous compounds. Very low and stringent drinking water limits have been placed on many halogenated organic compounds. For example, the maximum concentration limits for solvents such as trichloroethylene, tetrachloroethylene, and carbon tetrachloride have been established at 5 .mu.g/L, while the maximum concentration limits for chlorobenzenes, polychlorinated biphenyls (PCBs), and ethylene dibromide have been established by the USEPA at 100 .mu.g/L, 0.5 .mu./L, and 0.05 .mu.g/L, respectively. Meeting these cleanup criteria is difficult, time consuming, costly, and often virtually impossible using existing technologies.

The literature teaches the use of strong oxidizing agents to treat contaminated soil by chemically degrading recalcitrant and hazardous chemicals, either *in situ* or *ex situ*. Such oxidizers include Fenton's reagent, ozone, potassium permanganate and

30

- persulfates. One key aspect to the ability of an oxidizer to function is its ability to permeate through the subsurface, interacting with target compounds throughout the entire zone of contamination. Oxidizing species, such as peroxide, ozone and hydroxyl radicals have relatively short lifetimes within the subsurface. Persulfate radicals survive for greater periods. However there is a desire to have even longer lived active species available for organic species decomposition in order to increase the zone of reaction, without resorting to multiple injection points throughout the contamination area.
- It is commonly known that the reactivity of hydrogen peroxide, through the production of hydroxyl radicals, requires acid conditions. Typically acid is added with the hydrogen peroxide to increase the rate of reaction. Also, in many of its industrial uses, persulfate solutions are also kept under acidic conditions to increase their reactivity.
- Persulfates have been shown to oxidize a wide range of recalcitrant chemicals, and in combination with either heat or catalyst, are highly effective. However, it is known that during the course of oxidation by persulfate, the persulfate decomposition and reaction pathways generate sulfuric acid. One part of persulfate produces one part of sulfuric acid. If the buffering capacity of the nascent soil is not high enough, this acid production may yield a lowering of the ambient pH. While the acidic pH aids in the reactivity of the persulfate, low soil or ambient pH in the groundwater can be an issue, particularly resulting in the mobilization of toxic metals in the subsurface, causing an increase in oxidant decomposition rates, or requiring further remediation to meet regulated pH guidelines.

## SUMMARY OF THE INVENTION

- The present invention relates to a method for the treatment of contaminated soil, sediment, clay, rock, and the like (hereinafter collectively referred to as "soil") containing volatile organic compounds, semi-volatile organic compounds,

pesticides and herbicides, as well as the treatment of contaminated groundwater (i.e., water found underground in cracks and spaces in soil, sand and rocks), process water (i.e., water resulting from various industrial processes) or wastewater (i.e., water containing domestic or industrial waste, often referred to as sewage) containing these compounds.

The method of the present invention uses one or more water soluble oxidants in combination with a pH modifier, where the pH modifier maintains a pH greater than 9.0, under conditions which enable oxidation of most, and preferably substantially all, the organic compounds in the soil, groundwater, process water and/or wastewater, without the deleterious effects of metal mobilization or oxidant decomposition.

#### 15 BRIEF DESCRIPTION OF THE DRAWINGS

Fig 1 is a graph showing the relationship between the mole ratio of potassium hydroxide and persulfate reactivity.

Fig 2 is a table showing pH as a function of the mole ratio of potassium hydroxide to persulfate ions.

20 Fig 3 is a table showing 14 day results for destruction of various compounds for two different potassium hydroxide to persulfate mole ratios.

#### DESCRIPTION OF THE PREFERRED EMBODIMENTS

In accordance with the process of the present invention, organic compounds are oxidized by contacting the organic compound with a composition comprising (a) a water soluble peroxygen compound and (b) a pH modifier – i.e., any compound which is capable of maintaining the pH greater than 10 in its intended environment.

The oxidant may be any solid phase water soluble peroxygen compound, introduced into the soil or water in amounts, under conditions and in a manner which assures that the oxidizing compound is able to contact and oxidize most, and



preferably substantially all, the target compounds.

In a preferred embodiment of the invention a composition comprising potassium or sodium hydroxide and a peroxygen compound is introduced into the soil in  
5 sufficient quantities to satisfy the soil oxidant demand, compensate for decomposition, and to oxidize the target compounds. The quantity of the pH modifier that needs to be added is sufficient maintain the pH of at least 9 throughout the course of the contaminant decomposition by the peroxygen. This pH modification methodology may also be used ex situ to treat quantities of  
10 contaminated soil which have been removed from the ground.

According to another aspect of the present invention, under conditions where metal cations are present in the contaminated soil or water, the persulfate and hydroxide composition may be introduced into the contaminated soil to remove the target  
15 compounds. The metal cations catalytically decompose the persulfate to form sulfate free radicals, which oxidize the target VOCs. If the metal cations are not naturally present in sufficient quantities, they may be added from an external source. Such metal cations include divalent transition metals such as  $\text{Fe}^{+2}$ . Also, chelated metal ions, such as  $\text{Fe}^{+3}$  chelated with EDTA, where the chelant provides  
20 enhanced stability and solubility of the metal ion, may be added.

As per another aspect of the present invention, the persulfate and hydroxide composition may be introduced into the soil, followed by heating of the soil to  
25 activate the persulfate free radicals. Likewise, the persulfate and hydroxide composition may be introduced into soil that has already been pre-heated for activation of persulfate free radicals.

In one embodiment of the present invention, the oxidation of organic compounds at a contaminated site is accomplished by the injection of a combination of persulfate  
30 and a hydroxide into the soil.

In a preferred form of the invention, sodium persulfate (Na.sub.2 S.sub.2 O.sub.8) is introduced into the soil.

- 5 For in situ soil treatment, injection rates must be chosen based upon the hydrogeologic conditions, that is, the ability of the oxidizing solution to displace, mix and disperse with existing groundwater and move through the soil. Additionally, injection rates must be sufficient to satisfy the soil oxidant demand and chemical oxidant demand in a realistic time frame and to compensate for any
- 10 decomposition of the oxidant. It is advantageous to clear up sites in both a cost effective and timely manner. Careful evaluation of site parameters is crucial. It is well known that soil permeability may change rapidly both as a function of depth and lateral dimension. Therefore, injection well locations are also site specific. Proper application of any remediation technology depends upon knowledge of the
- 15 subsurface conditions, both chemical and physical, and the present process is not different in that respect.

While sodium persulfate is the preferred peroxygen compound for oxidizing soil constituents, other solid phase water soluble peroxygen compounds can be used. By "solid phase water soluble peroxygen compound" it is meant a compound that

20 is solid and water soluble at room temperature and contains a bi-atomic oxygen group, O--O. Such compounds include all the dipersulfates, monopersulfates, peroxides, and the like, with the dipersulfates being preferred because they are inexpensive and survive for long periods in groundwater saturated soil under typical site conditions.

- 25 The most preferred dipersulfate is sodium persulfate as it has the greatest solubility in water and is least expensive. Moreover, it generates sodium and sulfate upon reduction, both of which are relatively benign from environmental and health perspectives. Potassium persulfate and ammonium persulfate are examples of other persulfates which might be used. Potassium persulfate, however, is an order of
- 30 magnitude less soluble in water than sodium persulfate; and ammonium persulfate

is even less desirable as it may decompose into constituents which are potential health concerns.

In addition to potassium and sodium hydroxide, examples of other pH modifiers that may be used include phosphate compounds, such as sodium tripolyphosphate, and carbonate compounds, such as soda ash. The weight ratio of persulfate to hydroxide may be varied over a wide range depending upon the soil conditions and final target pH. A preferred ratio is 90 parts of persulfate and 10 parts of potassium hydroxide which is less than the stoichiometric requirement for acid neutralization. It is also preferred to combine the persulfate and hydroxide as a dry blend prior to shipment to the site where the composition is to be used. Thus it is desirable that the solid pH modifier be stable and non-hygroscopic. The hydroxide modifiers have such properties. However, it is also possible to combine the two ingredients to prepare the composition at the site. Alternatively, the persulfate and the pH modifier may be injected sequentially at the site and the composition formed in situ.

The persulfate and pH modifier, being compatible with each other, may be mixed together and shipped or stored prior to being combined with water in the same vessel prior to injection. It is preferred that enough persulfate is present to satisfy substantially all the soil oxidant demand and to destroy the target compounds to acceptable levels, or as close thereto as possible, and enough pH modifier is present to maintain a pH of at least 10.

Depending upon the type of soil, target compounds, and other oxidant demand by the site, the concentrations of persulfate used in the present invention may vary from 0.5 g/L to greater than 250,000 mg/L. The preferred concentrations are a function of the soil characteristics, including the site-specific oxidant demands. Hydrogeologic conditions govern the rate of movement of the chemicals through the soil, and those conditions must be considered together with the soil chemistry to understand how best to perform the injection. The techniques for making these determinations and performing the injections are well known in the art. For

example, wells or borings can be drilled at various locations in and around the suspected contaminated site to determine, as closely as possible, where the contamination is located. Core samples can be withdrawn, being careful to protect the samples from atmospheric oxidation. The samples can then be used to  
5 determine soil oxidant demand and chemical (e.g. VOC) oxidant demand and the oxidant stability existing in the subsurface. The precise chemical compounds in the soil and their concentration can be determined. Contaminated groundwater can be collected. Oxidants can be added to the collected groundwater during laboratory treatability experiments to determine which compounds are destroyed, in what  
10 order and to what degree, in the groundwater. It can then be determined whether the same oxidants are able to destroy those chemicals in the soil environment.

One method for calculating the preferred amount of peroxygen compound to be used per unit soil mass (for an identified volume of soil at the site) is to first  
15 determine the minimum amount of persulfate needed to fully satisfy soil oxidant demand per unit mass of uncontaminated soil. A contaminated soil sample from the identified volume of soil is then treated with that predetermined (per unit mass) amount of persulfate; and the minimum amount of peroxygen compound required to eliminate the organic compounds in that treated sample is then determined.  
20 Chemical reaction stoichiometry governs the mass/mass ratios and thus the total amount required to achieve the desired result. In actuality the amount of peroxygen compound injected into various locations at a single contaminated site will vary depending upon what is learned from the core samples and other techniques for mapping what is believed to be the subsurface conditions.

25 The goal is for the concentration of peroxygen compound in the injected solution to be just enough to result in the peroxygen compound reaction front traveling throughout the area of contamination requiring treatment in sufficient quantity to oxidize the contaminants present. (The saturated soil zone is the zone of soil which  
30 lies below the water table and is fully saturated. This is the region in which groundwater exists and flows.) In certain saturated soil zones where the natural

velocity of the groundwater is too slow for the purposes of treatment within a certain timeframe, the velocity of groundwater can be increased by increasing the flow rate of the injected solution or installation of groundwater extraction wells to direct the flow of the injected peroxygen compound solution. Certain soils to be treated may be in unsaturated zones and the method of peroxygen compound injection may be based on infiltration or trickling of the peroxygen compound solution into the subsurface to provide sufficient contact of the soils with the injected chemicals. Certain soils and conditions will require large amounts of peroxygen compound to destroy soil oxidant demand, while other soils and conditions might not. For example, sandy soils having large grain size might have very little surface area, very little oxidizable compounds and therefore very little soil oxidant demand. On the other hand, silty or clayey soils, which are very fine grained, would have large surface area per unit volume. They are likely to also contain larger amounts of oxidizable compounds and thus have a higher overall soil oxidant demand.

The amount of pH modifier used in the present invention may vary from those having a mole ratio of hydroxide ion to persulfate ion of from greater than 0.01 to less than 1.0 (the theoretical stoichiometric requirement). Preferred results are achieved with a hydroxide ion to persulfate ion mole ratio of from 0.10 to 0.8, especially preferred results are achieved at from about 0.4 to 0.8

In addition to in situ applications the process may also be employed ex situ. In addition to soil it may be used to treat sludges, sands, tars, groundwater, wastewater, process water or industrial water.

Another exemplary form of the invention is useful for destroying relatively low level, but unacceptable, concentrations of organic compounds in groundwater.

In order to describe the invention in more detail, the following examples are set forth:

#### EXAMPLES

Solid sodium persulfate and potassium hydroxide were added to 40 mL brown glass vials at the appropriate masses to obtain targeted concentrations

Distilled water was added to the vial to contain zero headspace and the  
5 vial was capped with a teflon lined silicon rubber screw top to prevent volatile loss

A mixture of the volatile organic compounds (in methanol) was injected through the septum of the sealed vials into the water/oxidant/activator mixture.  
10

Controls were constructed, without the addition of sodium persulfate, identical to the reaction vials

All vials were reacted at room temperature for 7 or 14 days.  
15

Following the 7 or 14 day reaction period, vials were stored at 4 deg C for analysis.

Analyses were performed on a gas chromatograph/mass spectrometer  
20 utilizing USEPA SW-846, Method 8260B

Reaction data were compared to control data in order to factor out any non-oxidative (i.e., volatile) losses that may have occurred

25 The reduction of organics results are shown in attached Figures 1 and 3. Similar vials containing different mole ratios of potassium hydroxide and persulfate were prepared and stored. The pH was measured after 7 and 14 days. The change in pH is shown in Figure 2.

What is claimed is:

1. A method for oxidizing an organic compound comprising contacting the organic compound with a composition comprising a water soluble peroxygen compound and a pH modifier which maintains the pH of the composition at greater than 10.
2. A method as in claim 1, wherein the organic compound is present in soil, groundwater, process water or wastewater.
3. A method as in claim 1, wherein the organic compound is selected from the group consisting of volatile organic compounds, semi-volatile organic compounds, polyaromatic hydrocarbons, polychlorobiphenyls, pesticides and herbicides.
4. The method as in claim 1, wherein the peroxygen compound is a dipersulfate.
5. The method as in claim 4, wherein the dipersulfate is selected from sodium, potassium or ammonium persulfate or a combination thereof.
6. The method as in claim 1, wherein the peroxygen compound is a monopersulfate.
7. The method as in claim 6, wherein the monopersulfate is selected from sodium and potassium monopersulfate.
8. The method as in claim 1, wherein the peroxygen compound is a combination of a dipersulfate and a monopersulfate.

9. The method as in claim 8 where the pH modifier is sodium hydroxide or potassium hydroxide
10. The method as in claim 9 wherein hydroxide and persulfate are added in combination so that the mole ratio of hydroxide ion to persulfate ion is greater than 0.01 but less than 1.0.
11. The method as in claim 10 wherein the hydroxide and persulfate are added in combination so that the mole ratio of hydroxide ion to persulfate ion is greater than 0.30 but less than 0.80.
12. The method as in claim 1 wherein the pH modifier is sodium hydroxide.
13. The method as in claim 1, wherein the composition is introduced into soil in sufficient quantities and under conditions to oxidize substantially all the volatile organic compounds in the soil.
14. The method as in claim 13, wherein the composition is introduced into the soil either *in situ* or *ex situ*.
15. The method as in claim 14, wherein the soil is heated to a temperature up to 99 degrees C.
16. A method for oxidizing organic compounds comprising contacting the compounds with a composition comprising a water soluble peroxygen compound, a pH modifier capable of maintaining a pH greater than 9, and a catalyst.
17. A method as in claim 16, wherein the organic compound is selected from the group consisting of volatile organic compounds, semi-volatile organic compounds, polyaromatic hydrocarbons, polychlorobiphenyls, pesticides and herbicides.
18. The method as in claim 16, wherein the peroxygen compound is a dipersulfate.



19. The method as in claim 18, wherein the dipersulfate is selected from sodium, potassium or ammonium persulfate or a combination thereof.
20. The method as in claim 16, wherein the peroxygen compound is a monopersulfate.
21. The method as in claim 20, wherein the monopersulfate is selected from sodium and potassium monopersulfate.
22. The method as in claim 16, wherein the peroxygen compound is a combination of a dipersulfate and a monopersulfate.
23. The method as in claim 16 wherein the pH modifier is potassium hydroxide.
24. The method as in claim 23 wherein hydroxide and persulfate are added in combination so that the mole ratio of hydroxide ion to persulfate ion is greater than 0.01 but less than 1.0.
25. The method as in claim 24 wherein the hydroxide and persulfate are added in combination so that the mole ratio of hydroxide ion to persulfate ion is greater than 0.10 but less than 0.30.
26. The method as in claim 16 wherein the pH modifier is sodium hydroxide.
27. The method as in claim 16 wherein the catalyst consists of a divalent or trivalent transition metal.
28. The method as in claim 16 wherein the catalyst consists of a divalent or trivalent transition metal in combination with a chelating agent.
29. The method as in claim 16, wherein the composition is introduced into soil in sufficient quantities and under conditions to oxidize substantially all the volatile organic compounds in the soil.

30. The method as in claim 28, wherein the composition is introduced into the soil either *in situ* or *ex situ*.
31. The method as in claim 29, wherein the soil is heated to a temperature up to 99 degrees C.

**Abstract**

Volatile organic compounds are removed from contaminated soil, groundwater and the like by treatment with a combination of a water soluble peroxygen compound, such as a persulfate, and a pH modifier capable of maintaining a pH greater than  
5 10, such as potassium hydroxide.

**Figure 1: Effect of KOH Ratio on Persulfate Reactivity**

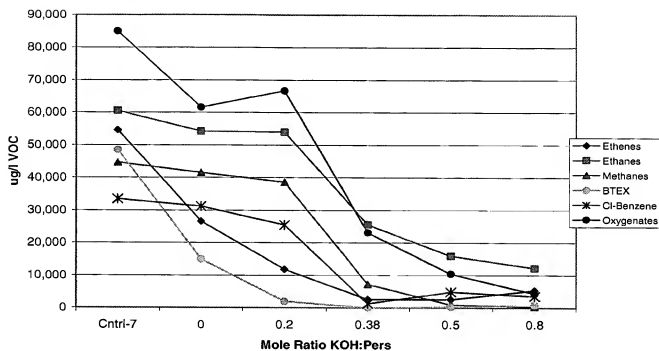


Figure 2: pH versus KOH mole Ratio		
Mole Ratio	pH, 7-days	pH, 14-days
0	1.3	0.5
0.2	4.3	4.5
0.38	11.5	10.4
0.5	11.5	10.5
0.8	12.2	13

Figure 3: Destruction of Recalcitrant Compounds with Alkaline Persulfate – Day 14 Results			
µg / L	Control Day 14	0.5 mol KOH : Persulfate	0.8 mol KOH : Persulfate
1,1,1-TCA	19,000	14,400	3,400
1,1,2-TCA	25,000	ND	ND
1,2-DCA	22,000	ND	ND
1,1-DCA	17,000	1,600	ND
Carbon Tetrachloride	18,000	ND	ND
Methylene Chloride	20,000	ND	ND
Vinyl Chloride	195	ND	ND
	ND – non detect		